Numerical simulation of turbulent sediment transport, from bed load to saltation.

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(Dated: September 13, 2011)

Sediment transport is studied as a function of the grain to fluid density ratio using two phase numerical simulations based on a discrete element method (DEM) for particles coupled to a continuum Reynolds averaged description of hydrodynamics. At density ratio close to unity (typically under water), vertical velocities are small so that sediment transport occurs in a thin layer at the surface of the static bed, and is called bed load. Steady, or 'saturated' transport is reached when the fluid borne shear stress at the interface between the mobile grains and the static grains is reduced to its threshold value. The number of grains transported per unit surface is therefore limited by the flux of horizontal momentum towards the surface. However, the fluid velocity in the transport layer remains almost undisturbed so that the mean grain velocity scales with the shear velocity u_* . At large density ratio (typically in air), the vertical velocities are large enough to make the transport layer wide and dilute. Sediment transport is then called saltation. In this case, particles are able to eject others when they collide with the granular bed, a process called splash. The number of grains transported per unit surface is selected by the balance between erosion and deposition and saturation is reached when one grain is statistically replaced by exactly one grain after a collision, which has the consequence that the mean grain velocity remains independent of u_* . The influence of the density ratio is systematically studied to reveal the transition between these two transport regimes. Based on the mechanisms identified in the steady case, we discuss the transient of saturation of sediment transport and in particular the saturation time and length. Finally, we investigate the exchange of particles between the mobile and static phases and we determine the exchange time of particles.

I. INTRODUCTION

After the pioneering works of Richardson [1], Rouse [2] and Vanoni [3], transport and dispersion of impurities suspended in turbulent flows, such as sand grains, dust, bubbles or droplets, have received a renewed interest in the last decade, both from the fundamental point of view [4–6] and for its applications to planetology [7], cloud physics[8] or geomorphology. In the later case, sediment may be entrained, transported and deposited by water flow or by wind. Then, gravity cannot be neglected as transport generically takes place in a turbulent boundary layer bounded by an erodible granular bed. Moreover, transported particles are not passively advected by the flow: they induce a negative feedback, which eventually limits the erosion of the granular bed, leading to a steady state in which erosion and deposition balance each other.

In such a homogeneous and steady situation, the fluid flow can be characterised by a unique quantity: the shear velocity u_* . The flux of sediments transported by the flow, called the saturated flux and noted q_{sat} , is an increasing function of u_* whatever the nature of the fluid. For aeolian transport, there has been a great effort to obtain the relation $q_{\text{sat}}(u_*)$ experimentally[9–19] using both wind tunnels and atmospheric flows in the field, numerically[20–22] and theoretically [10, 23–29]. Similarly, quite a number of expressions for subaqueous bedload have been proposed, e.g. [30–37]. Most models are based on the same dynamical mechanisms and differ only by the approximation used to compute the particle trajectories [38–42]. For this reason, experiments have been performed to determine the saltating motion of individual particles under water [43–47] and in air [48–51].

Despite this wide literature, some fundamental aspects of sediment transport are still partly understood. For instance, the dynamical mechanisms limiting sediment transport, and in particular the role of the bed disorder [52] and of turbulent fluctuations [53–60], remain a matter of discussion. Also, derivations of transport laws have a strong empirical or semi-empirical basis, thus lacking more physics related inputs. Here we investigate the properties of sediment transport using a novel numerical description of particle-laden flows. In particular, we examine the transition from bed-load to saltation by studying the influence of the grain to fluid density ratio.

The outline of the paper is the following. In section II, we introduce the equations of motion for the grains as well as the equations of hydrodynamics, emphasising the coupling between the two. Then, in section III, we detail the characteristics of saturated transport in the two limiting cases: bed load (water) and saltation (air). In section IV, we propose an interpretation of the simulations based on simple transport models. We then use these transport descriptions to derive and discuss out-of-equilibrium transport and in particlar the the saturation length and time (section V). We contrast this time with the 'exchange time', which characterises the diffusion of particles through the static/mobile interface. Finally, conclusions are outlined in the last section.

II. TRANSPORT MODEL

A. Key ideas

We wish to model the transport of non-cohesive grains by a flow, under gravity. Although a continuum two phase (grains and fluid) modelling [61] is very appealing, it is problematic by several aspects. (i) It postulates that particles constitute an Eulerian phase, which means that the particles crossing an arbitrary control volume have almost the same velocity. In a homogeneous steady flow, an Eulerian approach immediately predicts that particles are transported along the direction parallel to the bed and to the flow - vertical velocities are ignored. However, at least for saltation, they are essential. (ii) Such a continuum approach ignores the discrete and disordered nature of the granular phase. However, these properties are essential close to the transport threshold, below which no grain can be entrained. For instance, such models incorrectly predict the threshold shear velocity and in particular its strong decrease with the grain Reynolds number. To avoid these issues, we use here a discrete element method for the particles [20, 21, 62–64].

Solving hydrodynamics around grains is technically feasible only if the size of the domain (the number of grains) and the time over which the simulation is run are very small. The idea introduced here is thus to use a continuum description of hydrodynamics, averaged at a scale larger than the grain size. This means that the feedback of the particles on the flow is treated in the mean field manner.

This method allows one to perform very long numerical simulations (typically $1000 \sqrt{d/g}$, using large spatial domains (typically $1000 \ge 15$ grains), while keeping the complexity of the granular phase. We will now detail the different ingredients of the model. To avoid the formation of ordered structures in the grain packing, we have used a slightly polydisperse sample (20%). For the sake of simplicity, we only give here the equations for the strictly monodisperse case (grains of diameter d).

B. Forces on particles

1. Equations of motion

The grains have a spherical shape and are described by their dimensionless position vector \vec{r} , velocity \vec{v} and angular velocity $\vec{\omega}$ (see table I for units). A given grain labelled p inside a fluid obeys the dimensionless equations of motion,

$$m\frac{d\vec{u}^p}{dt} = -m\left(1 - \frac{\rho_f}{\rho_p}\right)g\vec{e}_z + \sum_q \vec{f}_{p,q} + s^{-1}\vec{f}_{\rm drag}^p$$

$$Imd^{2}\partial_{t}\vec{\omega}^{p} = \frac{1}{2}\sum_{q}\vec{n}_{p,q}\times\vec{f}_{p,q}$$
(1)

where \vec{e}_z is the vertical unit vector, I = 1/10 is the normalized moment of inertia of a sphere, $f_{p,q}$ is the contact force with grain q, $\vec{n}_{p,q} = (\vec{r}^q - \vec{r}^p)/|\vec{r}^q - \vec{r}^p|$ is the contact direction and \vec{f}_{drag}^p is the drag force.

2. Contact forces

Following a standard approach for the modeling of contact forces in MD codes, see [65–68] and references therein, we consider the case where grains in contact are subject to (i) normal repulsion, (ii) tangential friction and (iii) energy dissipation. For simplicity, the normal repulsion is given by a spring-like elastic force, which is a good approximation for very small contact deformations. The tangential friction is modeled by a tangential elastic force proportional to the relative tangential displacement between the grains. The moment of this force can induce particle rotation. Whenever the tangential exceeds a given fraction of the normal force, defined by a microscopic friction coefficient, the contact 'slides' (Coulomb friction law). Finally, energy dissipation at the contact is ensured by adding a damping term to the force, proportional to the relative contact velocity. This term accounts for the restitution coefficient e, i.e. the ratio between grain velocities after and before a collision.

3. Drag force

We hypothesise here that the drag force exerted by the fluid on a moving grain depends only on the difference between the grain velocity \vec{u}^p and the fluid velocity \vec{u} around it. This assumption is valid if the turbulent fluctuations of the flow itself can be neglected in front of those induced by the grain. Introducing the particle Reynolds number R_u based on this fluid-particle velocity difference $R_u = |\vec{u} - \vec{u}^p| d/\nu$, the drag force can be written under the form

$$\vec{f}_{\rm drag}^p = \frac{\pi}{8} \rho_f d^2 C_d(R_u) |\vec{u} - \vec{u}^p| (\vec{u} - \vec{u}^p)$$
(2)

where $C_d(R_u)$ is the drag coefficient. We use the following convenient phenomenological approximation [?]:

$$C_d(R_u) = \left(\sqrt{C_d^{\infty}} + \sqrt{R_u^c/R_u}\right)^2 \tag{3}$$

where $C_d^{\infty} \simeq 0.5$, is the drag coefficient of the grain in the turbulent limit $(R_u \to \infty)$, and $R_u^c \simeq 24$ is the transitional particle Reynolds number above which the drag coefficient becomes almost constant. The lift force and the corrections to the drag force (Basset, added-mass, etc) are neglected.

C. Hydrodynamics

Hydrodynamics is described by the Reynolds averaged Navier-Stokes equations:

$$\rho_f \left(\partial_t u_i + u_j \partial_j u_i \right) = -\partial_i p + \rho_f g_i + \partial_j \tau^f_{ij} - F_i.$$
(4)

In this expression, τ_{ij}^f is the total stress tensor resulting both from viscous diffusion of momentum (viscous stress) and transport of momentum by turbulent fluctuations (Reynolds stress). F_i is the body force exerted by the grains on the fluid. It reflects the turbulent fluctuations induced by a moving grain, which can be non-local. As we focus in this paper on steady homogeneous sediment transport, we hypothesise that the influence of a given grain remains localised in a thin horizontal region and that the typical horizontal distance over which the flow is disturbed is comparable to the distance between moving grains. $F_x(z)$ can then be obtained by averaging the horizontal component of the drag $f_{\text{drag }x}^p$ acting on all the grains moving around altitude z, in a horizontal layer of area A and of thickness dz:

$$F_x(z) = \frac{1}{Adz} \left\langle \sum_{p \in \{z; z+dz\}} f^p_{\operatorname{drag} x}(z) \right\rangle.$$
 (5)

The $\langle . \rangle$ denote here the ensemble averaging. In order to gain statistics, we make use of the steady character of the studied situation, and also use time averaging. For simplicity, we write $\tau^f = \tau^f_{xz}$ the fluid shear stress. The horizontal component of the Reynolds equation reduces to $\partial_z \tau^f = F_x$, which can be integrated in

$$\tau^{f}(z) = \rho_{f} u_{*}^{2} - \tau^{p}(z) \tag{6}$$

where we have introduced the shear velocity u_* and the grain borne shear stress τ^p thus defined by

$$\tau^{p}(z) \equiv \int_{z}^{\infty} dz' F_{x}(z') = \frac{1}{A} \left\langle \sum_{p \in \{z' > z\}} f^{p}_{\operatorname{drag} x}(z') \right\rangle.$$
(7)

In order to relate the fluid borne shear stress to the average velocity field, we adopt Prandtl's turbulent closure [69]. Introducing the turbulent mixing length ℓ , we write

$$\tau^f = (\nu + \ell^2 |\partial_z u_x|) \partial_z u_x \tag{8}$$

We know that ℓ should vanish below some critical Reynolds number R_c and should be proportional to the distance to the ground z, far above the transport layer. We have used a phenomenological differential equation to formulate the mixing length

$$\frac{d\ell}{dz} = \kappa \left[1 - \exp\left(-\sqrt{\frac{1}{R_c} \left(\frac{u\ell}{\nu}\right)}\right) \right] \tag{9}$$

where $\kappa \simeq 0.4$ is von Karman's constant. Here R_c is fixed to 17. The ratio $u\ell/\nu$ is the Reynolds number based on

General	
length l	d
acceleration	g
time t	$\sqrt{d/g}$
velocity v	\sqrt{gd}
Particles	
angular velocity ω	$\sqrt{g/d}$
mass m	$\sqrt{g/d} \ rac{\pi}{6} ho_p d^3$
moment of inertia I	md^2
force f	mg
contact stiffness k	mg/d
damping constant γ	$m\sqrt{g/d}$
Fluid	
shear stress τ	$(\rho_p - \rho_f)gd$

grain diameter (d)

the mixing length. Note that any other function than the exponential can be used, provided it has the same behaviour in 0 and $-\infty$ (see appendix for more details). This formulation allows us to define ℓ both inside and above the static granular bed. Interestingly, there is no need to define explicitly an interface between static and mobile zones.

D. Dimensionless numbers

As must be the case in any numerical simulation, the equations are made dimensionless. Gravity gives the relevant scale for forces. More precisely, it only appears in the grain equation of motion under the form of a buoyancy-free gravity $\left(1 - \frac{\rho_f}{\rho_p}\right)g$. The choice of the typical length scale is less obvious. On the one hand, the contact forces and the trapping of particles at the surface of the bed do not depend on the fluid properties: the grain diameter d is thus the relevant length scale for the static grains. On the other hand, one can build a drag length from hydrodynamic, which is the length needed to accelerate a grain to the fluid velocity. This inertial length scales as $\frac{\rho_p}{\rho_f} d$ and is the relevant length scale for the mobile grains. This means that the density ratio ρ_p/ρ_f cannot be eliminated and is a true dimensionless parameter of the problem. We shall see below that this density ratio is the parameter controlling the transition from bed load to saltation. We have chosen das a reference length scale, and Table I summarises all the parameters used to make the problem dimensionless in our code. The second control parameter is the shear velocity u_* imposed far from the bed, or equivalently the shear stress $\rho_f u_*^2$. Its dimensionless counterpart is the

Shields number [70], defined by

$$\Theta = \frac{\rho_f u_*^2}{(\rho_p - \rho_f)gd} , \qquad (10)$$

which encodes the strength of the flow. Making the viscosity non-dimensional, we obtain a grain-based Reynolds number

$$R_e = \frac{d}{\nu} \sqrt{\left(\frac{\rho_p}{\rho_f} - 1\right)gd} \tag{11}$$

Physically, it determines the hydrodynamic regime at the scale of the grain. The figures presented in this paper are obtained for the same particle Reynolds number $R_e = 10$. This value is sufficiently large to ensure that the grain diameter is much larger than the viscous sub-layer size. As a consequence, the flow is fully turbulent at all the scales of the problem. It becomes viscous below the first layer of static grains.

Dynamics at the scale of the contact between grains is controlled by different dimensionless numbers: the restitution coefficient e, the friction coefficient μ and the contact duration $t_c = \pi \sqrt{\frac{g}{(2k-\gamma^2)d}}$. We have checked that the values given to these parameters do not change qualitatively the results.

III. SATURATED TRANSPORT

A. Qualitative results

Transport equations are integrated until a statistically steady homogeneous state is reached. Since we are primarily interested in the transition from bed load to saltation, we have varied the Shields number within the range $\Theta = 0.003$ -0.7 (a range which contains the threshold Θ_d , see below) and the density ratio within the range $\rho_p/\rho_f = 2$ -2000.

Once transport has reached its saturated state, the general picture is as follows: at small density ratios $\rho_p/\rho_f \simeq 2$, which is the typical value underwater, the transport is confined at the surface, within a couple grain diameters. The dense and thin transport layer is characteristic of the bed load regime. On the contrary, at a large density ratio $\rho_p/\rho_f \simeq 2000$, which is typical of aeolian situation, the transport layer becomes wide and dilute, extending over several tens of grain diameters (Fig. 1). This is typical of the saltation regime. Within the very same numerical model, we are thus able to reproduce the basic characteristics of transport in both limits.

B. Saturated flux

Steady and homogeneous sediment transport is basically quantified by the volumetric saturated flux q_{sat} , i.e.

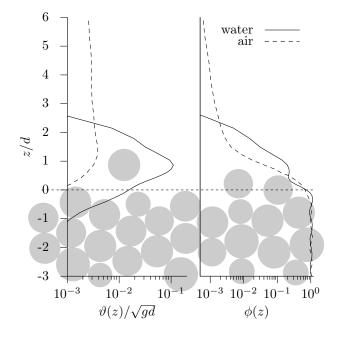


FIG. 1: Transport profiles: volume flux density $\vartheta(z)$ (solid lines) and volume fraction $\phi(z)$ (dashed lines) for water (red) and air (green).

the volume of the particles (at the bed density) crossing a vertical surface of unit transverse size per unit time. It has the dimension of m^2/s . In the simulations, we compute it as

$$q_{\rm sat} = \frac{1}{A\phi_b} \frac{\pi}{6} d^3 \sum_p u^p, \qquad (12)$$

where ϕ_b is the volume fraction of the static bed. A key issue is the dependence of $q_{\rm sat}$ on the shear velocity or, equivalently, on the Shields number Θ . In order to highlight this dependence, figure 2 shows the saturated flux rescaled by u_*^2 in both cases (water and air). In agreement with experimental observations [19, 30–34, 37, 71– 74], we find that $q_{\rm sat}$ scales asymptotically as Θ (or u_*^2) for saltation, while $q_{\rm sat}$ scales as $\Theta^{3/2}$ (or u_*^3) underwater (Fig. 2). Importantly, most models of aeolian transport miss the influence of the negative feedback of transport on the flow. Therefore, they do not give the correct scaling, predicting $q_{\rm sat} \propto u_*^3$. We unravel below, in the same numerical model, a fundamental difference between the two transport regimes, which correspond to different underlying dynamical mechanisms.

Figure 2 reveals the existence of a threshold shear velocity below which the flux vanishes. More precisely, we define the dynamical threshold Shield number Θ_d from the extrapolation of the saturated flux curve to 0, which gives in our case $\Theta_d \simeq 0.12$ for water $(\rho_p/\rho_f = 2)$ and $\Theta_d \simeq 0.004$ for air $(\rho_p/\rho_f = 2000)$, respectively. These values are consistent with experimental ones within a factor of 2. A refined tuning of these values could be

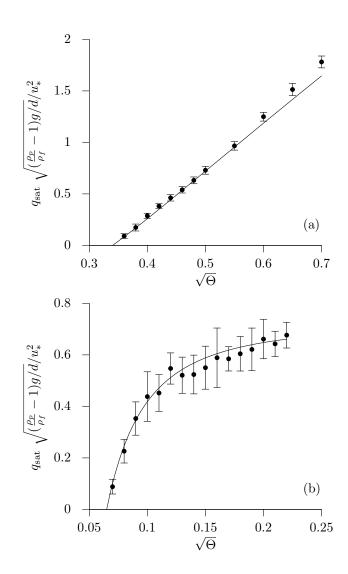


FIG. 2: Rescaled saturated flux $q_{\rm sat}\rho_p \sqrt{g/d}/\rho_f u_*^2$ versus the rescaled shear velocity $\sqrt{\Theta}$ for water (a) and air (b). For air the saturated flux scales asymptotically as Θ while for water it follows $\Theta^{3/2}$. Full lines are the predictions of the simplified models for bed load (Eq. 24) and saltation (Eq. 30), given in the text.

achieved by adjusting the value of R_c and by performing 3D simulations. Figure 3 shows the dependence of Θ_d with the density ratio ρ_p/ρ_f . It is usually assumed that the Shields number compares directly the horizontal force exerted on a surface grain to its weight, in which case the threshold Shields number could be interpreted as an effective friction coefficient, within a numerical factor. If this was true, Θ_d would be a constant, independent of ρ_p/ρ_f . However, one observes that Θ_d decreases rapidly with the density ratio.

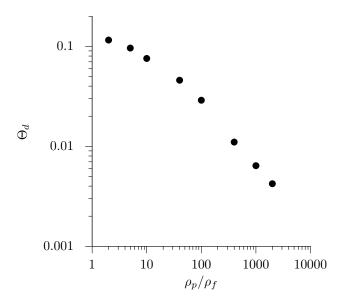


FIG. 3: Dynamical threshold Shield number Θ_d as a function of the density ratio ρ_p/ρ_f .

C. Transport layer

Figure 4 presents the vertical profiles of the flux density, i.e. the flux per unit height $\vartheta(z)$ (such that $q_{\text{sat}} \equiv \int \vartheta(z)dz$) for different shear velocities. It shows that bed load and saltation mainly differ by the vertical characteristics of the transport layer. At small density ratios the motion of grains is confined within a thin layer of few grain diameters (Fig. 4 a). Most of the bed load occurs at about one grain diameter above the static bed and the flux density profile decays symmetrically on both sides of this maximum. By contrast, for large density ratios, grains experience much higher trajectories and the transport layer is much wider. Figure 4b shows that the flux density still presents a maximum close to the static bed but decreases exponentially with height.

These qualitative observations can be formalized by defining a characteristic transport layer thickness λ from the flux density profile $\vartheta(z)$ as:

$$\lambda = \left(\frac{\int_0^\infty (z - \bar{z})^2 \,\vartheta(z)dz}{q_{\text{sat}}}\right)^{1/2} \tag{13}$$

where $\bar{z} = \frac{1}{q_{\text{sat}}} \int_0^\infty z \,\vartheta(z) dz$ gives the altitude of the transport layer centre. If the flux profile decreases exponentially, λ is the characteristic distance over which this decrease takes place. The variations of λ with the shear velocity are presented in the insets of figure 4. For underwater bed load, the size of the transport layer is about one grain diameter, gently increases with the shear velocity from $\lambda \simeq d/2$ to $\lambda \simeq d$. For aeolian saltation the transport layer is indeed wider, with a characteristic size $\lambda \simeq 50d$ roughly independent of the shear velocity.

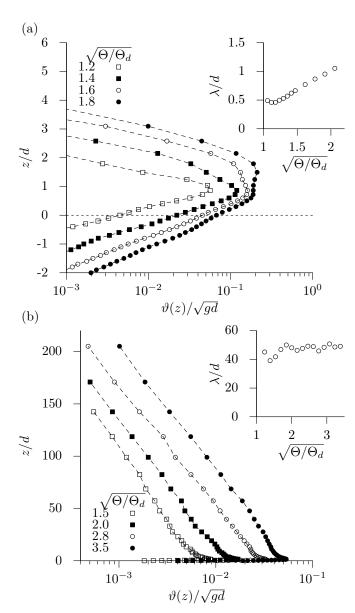


FIG. 4: Vertical profiles of the sediment flux density $\vartheta(z)$ for different values of the shear velocity ratio $\sqrt{\Theta/\Theta_d}$, in water (a) and air (b). The reference height z = 0 denotes the position of the bed surface. Insets: characteristic transport layer thickness λ as function of the shear velocity.

Figure 5 shows the dependence of the transport layer thickness λ with the density ratio. At large density ratio, λ is observed to scale with the drag length $\frac{\rho_p}{\rho_f}d$ which is the length that naturally emerges when the motion of the grains is dominated by the balance between inertia and hydrodynamical drag. This length is thus expected to control the characteristic hop height and hop length, which naturally leads to wider transport layers for lighter fluids.

Nevertheless, the transition from bed load to saltation is slightly more complex as λ does not strictly obey the

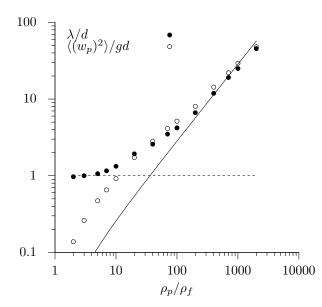


FIG. 5: Characteristic transport layer thickness λ (•) as function of the density ratio for $\Theta = 2\Theta_d$. At small density ratios it is limited by the grain size (dashed line), while for large ones it scales as ρ_p/ρ_f (solid line). The averaged vertical energy per grain $\langle (w^p)^2 \rangle / g$ (\circ) is also shown to illustrate the dynamical origin of λ (see text).

simple scaling law $\lambda \propto \frac{\rho_p}{\rho_f} d$. In sub-aqueous conditions, the transport layer thickness is actually limited by the grain size $\lambda \sim d$, which is the characteristic length scale for contact forces and geometrical trapping of particles [76, 77]. The hop height can be estimated from the particle vertical velocity w^p using the ballistic approximation, neglecting the vertical component of the drag force. Under this hypothesis, one expects the hop height to increase like $(w^p)^2/g$. Figure 5 shows the dependence of the average squared vertical velocity $\langle (w^p)2 \rangle$ on the density ratio. One observes that the transport layer thickness λ is determined by the hop length $\langle (w^p)^2 \rangle / g$ for $\rho_p / \rho_f \gtrsim 10$. Below this cross-over value, the transport layer thickness is given by the grain diameter d, although the trajectories are almost horizontal. The transition from bed load to saltation therefore takes place when the vertical velocities of the particles are sufficiently large for these particles to escape the traps formed by the grains of the static bed. Formally, the criterion of this transition can then be written as $\sqrt{\langle (w^p)^2 \rangle} \simeq \sqrt{gd}$.

IV. INTERPRETATION

A. A simple transport model for bedload

We propose here a simple model of bed load inspired from Bagnold's original ideas [32]. We hypothesise that moving grains are confined in a thin layer of thickness on the order of d. As the average particle vertical velocity is very small, grain hop heights are typically much smaller than d (Fig. 5), which means that the vertical motion of the grains can effectively be neglected. The saturated flux can then be decomposed as the product of the number n of transported grains per unit area by the mean grain horizontal velocity \bar{u}^p :

$$q_{\rm sat} = \frac{1}{\phi_b} \frac{\pi}{6} d^3 n \bar{u}^p. \tag{14}$$

In the numerical simulations, we compute n and \bar{u}^p as

$$n = \frac{\left(\sum_{p} u_{p}\right)^{2}}{A \sum_{p} u_{p}^{2}},$$
(15)

$$\bar{u}^p = \frac{\sum_p u_p^2}{\sum_n u_p},\tag{16}$$

where A is the surface area. Notice that these definitions are consistent with the definition of q_{sat} (12). If all grains were moving at the same velocity, then n and u^p would indeed be respectively the density of moving grains and their velocity.

We write that the grain born shear stress is proportional to the moving grain density n and to the drag force acting on a grain moving at the average velocity \bar{u}^p due to a flow at the velocity u:

$$\tau^p = nf_d \quad \text{with} \quad f_d = \frac{\pi}{8} C_d^\infty \rho_f \left(u - \bar{u}^p\right)^2 d^2.$$
 (17)

Here, for the sake of the argument, we neglect the dependence of the drag coefficient on the particle Reynolds number (see Eq. 3). A key assumption now is that grains are in a steady motion, which means that the drag force f_d balances a resistive force due to friction, to collisions with the bed, and to viscous lubrication forces. These different dissipative mechanisms can be modelled as an overall effective friction force characterized by a friction coefficient μ_d :

$$f_d = \frac{\pi}{6} \mu_d (\rho_p - \rho_f) g d^3.$$
 (18)

We can furthermore express the fluid velocity u_d at the transport threshold by assuming that the hydrodynamic drag exerted on a static grain $(u^p = 0)$ has to overcome a static friction, characterized by a coefficient μ_s :

$$u_d = \sqrt{\frac{4\mu_s}{3C_d^{\infty}} \left(\frac{\rho_p}{\rho_f} - 1\right)gd} .$$
 (19)

For later use, we define the corresponding threshold Shields number Θ_d as

$$\Theta_d = \frac{\rho_f u_d^2}{(\rho_p - \rho_f)gd} \,. \tag{20}$$

Combining the above equations shows that the velocity difference between the grain and the flow is constant:

$$\bar{u}^p = u - \sqrt{\frac{\mu_d}{\mu_s}} u_d \tag{21}$$

We now assume that the transported grains do not disturb the flow. Then, the flow velocity around grains u must be proportional to the shear velocity, so that $u/u_d = \sqrt{\Theta/\Theta_d}$. One therefore deduces:

$$\bar{u}^p = u_d \left(\sqrt{\frac{\Theta}{\Theta_d}} - \sqrt{\frac{\mu_d}{\mu_s}} \right) \,. \tag{22}$$

This predicts that the grain velocity does not vanish at the threshold, if friction is lowered during motion. The velocity at threshold $u_d(1 - \sqrt{\mu_d/\mu_s})$ can be interpreted as the velocity needed by a grain to be extracted from the bed and entrained by the flow.

Saturation is reached when the fluid shear stress reaches the transport threshold at the surface of the static bed i.e. when $\tau^p = \rho u_*^2 - \tau_d$. As consequence, the number of transported particles per unit area is solely determined by the excess shear stress:

$$n = \frac{\rho u_*^2 - \tau_d}{f_d} = \frac{\Theta - \Theta_d}{\frac{\pi}{6}\mu_d d^2}.$$
 (23)

Finally, the saturated flux reads:

$$q_{\text{sat}} = \frac{u_d d}{\phi_b \mu_d} \ \left(\Theta - \Theta_d\right) \ \left(\sqrt{\frac{\Theta}{\Theta_d}} - \sqrt{\frac{\mu_d}{\mu_s}}\right). \tag{24}$$

Inserting the expression (19) of u_d , one gets the scaling law for the flux at large Θ :

$$q_{\rm sat} \propto \Theta^{3/2} \sqrt{\left(\frac{\rho_p}{\rho_f} - 1\right)gd^3}$$
. (25)

B. A simple transport model for saltation

We now proceed in a similar manner for the aeolian saltation regime, following ideas initially proposed by Owen (1964) and Ungar & Haff (1987). In this regime, the motion of the grains is not confined to a thin layer at the surface of the bed. We consider an average grain trajectory, in which the particle takes off the bed with the horizontal velocity \bar{u}^p_{\uparrow} , and comes back to it with a velocity \bar{u}^p_{\downarrow} , after a hop of length *a*. Some momentum is extracted from the wind flow by the grains to perform their jumps, so that the particle shear stress writes

$$\tau^p = \rho_p \phi_b \frac{\bar{u}^p_{\downarrow} - \bar{u}^p_{\uparrow}}{a} q_{\text{sat}}.$$
 (26)

Now we use again the decomposition of the saturated flux as the product of the grain density n and the grain velocity \bar{u}^p (Eq. 14). Saturated transport corresponds to the balance $\tau^p = \rho_f u_*^2 - \tau_d$ so that n still has the same form as in the bed-load case:

$$n = \frac{(\rho_p - \rho_f)gd}{f_d} \left(\Theta - \Theta_d\right), \qquad (27)$$

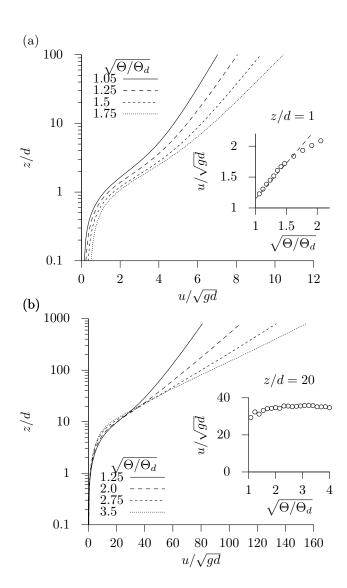


FIG. 6: Flow velocity vertical profiles at different shear velocity ratios $\sqrt{\Theta/\Theta_d}$ for water (a) and air (b). Insets: velocity at z = d and z = 20d respectively, as a function of the rescaled shear velocity. The dashed line in the upper inset corresponds to the fit $u \propto u_*$.

but with a different effective drag force f_d , not related to friction anymore but to grain velocities. As the grain hop length can be related to the grain velocity as $a \propto \bar{u}_{\uparrow}^p \bar{w}_{\uparrow}^p / g$ (balistic approximation), we can effectively write

$$f_d \propto \frac{\pi}{6} d^3 \rho_p g \, \frac{\bar{u}^p_{\downarrow} - \bar{u}^p_{\uparrow}}{\bar{w}^p_{\uparrow}} \, \frac{\bar{u}^p}{\bar{u}^p_{\uparrow}} \,. \tag{28}$$

Now, for saltation, steady transport also implies that the number of grains expelled from the bed into the flow exactly balance those trapped by the bed, i.e. a replacement capacity equal to one. Due to the grain feedback on the flow, in contrast with bed load, grains in the transport layer feel a flow independent of the wind strength

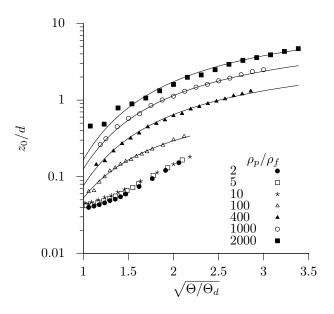


FIG. 7: Rescaled hydrodynamical roughness length as function of the shear velocity for different density ratios. Solid lines are the predictions based on the focal point assumption (Eq. 31).

(see Fig. 6 (b) below) and new moving grains thus come only from high energy bed collisions. Since the number of ejected grains is function of the impact energy (or equivalently on the impact velocity), the mean grain velocity \bar{u}^p must be constant, independently of the shear velocity, scaling with u_d :

$$\bar{u}^p \propto u_d.$$
 (29)

From this argument, it follows that all particle surface velocities $(\bar{u}^p_{\downarrow}, \bar{u}^p_{\uparrow}, \bar{w}^p_{\uparrow})$ also scale with u_d , so that f_d is also a constant. Finally, the scaling law followed by the saturated flux becomes,

$$q_{\rm sat} \propto (1 - \rho_f / \rho_p) u_d d \left(\Theta - \Theta_d\right). \tag{30}$$

C. Comparison with simulations

The above simple models suggest simple test to investigate the dynamical mechanisms in the DEM simulation. (i) Is saturation of transport due (or not) to the negative feedback of moving grains on the fluid? (ii) Do we recover the linear relation between the grain density n and the excess Shield number $\Theta - \Theta_d$, whatever the transport rgime. (iii) Does the mean grain velocity u^p depend (or not) on the shear velocity?

1. Grain feedback on the flow

The information of the feedback for the moving grains on the fluid flow is formally encoded in the flow roughness

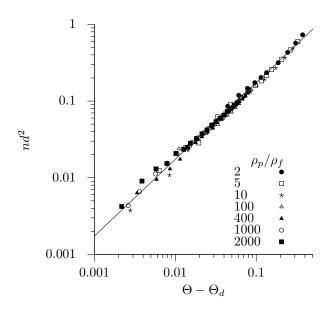


FIG. 8: Linear relation between the rescaled number of transported grains per unit area and the rescaled excess of shear stress for different density ratios.

length z_0 . However, it can first be qualitatively understood from the shape of the flow velocity profile inside the transport layer (Fig. 6). For bed load, as shown in the inset of Fig. 6 (a), the flow velocity at $z \simeq d$, where most of transport takes place, increases with the shear velocity. This indicates that the flow is barely disturbed. In contrast, for aeolian transport (Fig. 6 (b)) the flow velocity is strongly affected by the motion of grains as it becomes almost independent of the wind in the region $z \leq 20d$, which accounts for most of the transport layer.

The data of the hydrodynamical roughness length z_0 show a similar, or rather more complete, picture (Fig. 7). In the saltation regime the roughness length increases with the shear velocity as a result of grain feedback, which can be modeled from the existence of a focal point where $u = U_f$ at $z = H_f$ independently of u_* (Fig. 6 b), and above which the flow velocity recovers its log profile $u = u_*/\kappa \ln(z/z_0)$. This gives

$$z_0 \simeq H_f \exp\left(-\kappa U_f/u_*\right). \tag{31}$$

This expression fits rather well the increase of z_0 for stronger winds, when the density ratio ρ_p/ρ_f is large enough (Fig. 7). Typically below $\rho_p/\rho_f \simeq 10$, Eq. 31 does not reproduce the data anymore. This is consistent with the absence of a focal point in the bed load regime (Fig. 6 a). Also, in the small ρ_p/ρ_f limit, the roughness length remains very small (substantially smaller than d).

2. Number of transported grains and average grain velocity

From expressions (15) and (16), we can compute the number of transported grain per unit area and the mean

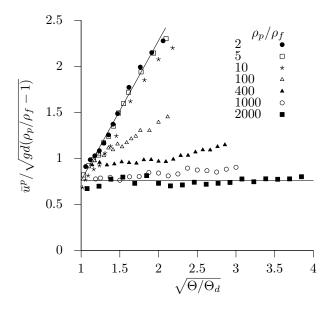


FIG. 9: Rescaled mean grain velocity as function of the rescaled the shear velocity for different density ratios. Full lines show the analytical prediction given in the text for the two limiting cases: water (Eq. 22) and air (Eq. 29).

grain horizontal velocity as a function of the shear velocity of the flow. Figure 8 shows a linear relation between n and $\Theta - \Theta_d$ for both bed load and saltation. This is consistent with the predictions of the above models. Interestingly, the friction coefficient μ_d , defined from the proportionality factor (see Eq. 23), has the same value $\simeq 1$ in both cases. This suggests that dissipation due to collisions of the moving grains with the bed plays the same role in both transport regimes.

The dependence of the mean grain velocity \bar{u}^p is also fully consistent with the picture emerging from the simple models. As shows in Fig. 9, \bar{u}^p increases linearly with $\sqrt{\Theta/\Theta_d}$ for bed load (Eq. 22) while it remains roughly constant for aeolian saltation (Eq. 29). Interestingly, the different curves shown in Fig. 9 cross at $\Theta = \Theta_d$. In other words, the grain velocity at the transport threshold scale on $\sqrt{gd(\rho_p/\rho_f - 1)}$, with a prefactor slightly smaller than unity, whatever the transport regime. This common behaviour between bed-load and saltation results from the fact that the negative feedback of transport on the flow disappears at the threshold, as n vanishes.

Fitting the grain density and the mean grain velocity to the simple model of bedload, one can extract the effective friction coefficients μ_d and μ_s . The static friction coefficient μ_s turns out to be $\simeq 4$ times larger than the dynamical friction coefficient μ_d . This means that the motion is lubrified by the fluid once grain are entrained. Therefore, the grain velocity at the threshold remains finite (but *n* vanishes).

V. SATURATION TRANSIENT

Beyond the properties of steady and homogeneous transport, we address in this section the time and length scales involved in the relaxation of the sediment flux toward its saturated value, which are relevant in the context of pattern formation [78–83]. We furthermore emphasize the difference between the saturation time and the exchange time.

A. Saturation length and time

Whatever the transport regime, the saturation transient is controlled by two mechanisms. On the one hand, bed erosion or deposition must take place to adapt the number of transported grains to the flow velocity. On the other hand, grains must be accelerated by the flow to their asymptotic velocity.

The authors have addressed the case of saltation in a series of articles, starting from a controversy between us [79, 87, 88] and resolving it [89]. In summary, the horizontal acceleration of a grain entrained by the wind is governed by the equation of motion:

$$\frac{\mathrm{d}u^{p}}{\mathrm{d}t} = \frac{3}{4} \frac{C_{d}^{\infty} \rho_{f}}{\rho_{p} d} (u - u^{p})^{2}.$$
(32)

Contrarily to bed load, in the saltation regime, dissipation only takes place during collisions and not through a permanent friction on the static bed. The only length scale in this equation is the so-called drag length $\frac{\rho_p}{\rho_f}d$. As a consequence, the relaxation of the particle velocity to the fluid velocity occurs over a length which varies as

$$L_{\rm sat} \propto \frac{\rho_p}{C_d^{\infty} \rho_f} d,$$
 (33)

independently of the wind speed, with a proportionality factor that depends on the restitution coefficient e[73]. Except in the vicinity of the transport threshold, the length over which the number of grains transported relaxes to its saturated state is much shorter than the drag length – it decays as u_*^{-2} . Therefore, the overall saturation length is proportional to the drag length, as confirmed by direct measurements [84].

The case of bed-load is still under debate [37, 52, 82]. We derive here saturation time and the saturation length in the simple bed-load model detailed above. As the moving grains form a surface layer of thickness d, the number of moving particles per unit area adapts immediately to a change of shear velocity. By contrast, the grain velocity relaxes to its asymptotic value with a characteristic time. This is what gives the saturation time. Neglecting for the sake of simplicity the dependence of the drag coefficient on the particle Reynolds number, the horizontal component of the grain equation of motion reads:

$$\frac{du^p}{dt} = \frac{3C_d^{\infty}\rho_f}{4\rho_p d} \left[(u - u^p)^2 - \frac{\mu_d}{\mu_s} u_d^2 \right].$$
 (34)

Linearising this equation around the asymptotic value, we obtain the following expression for the saturation time:

$$T_{\rm sat} = \sqrt{\frac{\mu_s}{\mu_d}} \, \frac{2\rho_p d}{3C_d^{\infty} \rho_f u_d} \,. \tag{35}$$

Using expression (19) for u_d and typical values for the various parameters, we get $T_{\rm sat}$ on the order of few $\sqrt{d/g}$. The saturation length is then the length over which the grain moves during $T_{\rm sat}$ at velocity \bar{u}^p :

$$L_{\text{sat}} = \frac{2}{3} \frac{\rho_p d}{C_d^{\infty} \rho_f} \left(\sqrt{\frac{\mu_s}{\mu_d}} \frac{u}{u_d} - 1 \right).$$
(36)

Inserting again typical numbers in this expression, we get, for u close to u_d , a value for L_{sat} on the order of few grain diameters. This is consistent with indirect measurements of the saturation length based on the initial wavelength of sub-aqueous ripples [82]. Preliminary simulations of transport over a sinusoidal sand bed also confirm this order of magnitude.

B. Exchange time vs saturation time

An important problem that cannot be tackled using the simple transport model presented here (or any Eulerian continuous model) is the exchange between the mobile and the static phases. Indeed, such a model does not aim to describe the lagrangian pathes of individual grains. In particular, recent studies have focused on the characteristic time a given grain spend in the transport layer before being trapped by the bed [37, 52, 82]. This time, noted $T_{\rm ex}$ hereafter, is either called the deposition time or the exchange time. It is relevant in geology as it is reflects the time scale associated with storage and reworking of sediments. The residence time should a priori not be confused with the saturation time. Imagine for instance the case where all the grains in the transport layer would move with a uniform and perfectly horizontal velocity. Then there would be no exchange with the static phase and $T_{\rm ex}$ would be infinite, although transport could reach saturation after a very short time. Despite this conceptual difference, the formalism proposed in [52] leads to the identity between the exchange time and the saturation time.

Using our granular based transport simulations, we address here this issue for bed load $(\rho_p/\rho_f = 2)$ by tracking all grains with velocities above a certain value at t = 0. For the sake of the discussion, we have chosen this value to be $\sqrt{gd}/2$, which allows us to determine the grains inside the transport layer at this initial time. Noting this particle ensemble \mathcal{E} , we define the density n_t of transported grains at time t = 0 that remains in the transport layer after a time t:

$$n_t = \frac{\left(\sum_{p \in \mathcal{E}} u_p\right)^2}{A \sum_{p \in \mathcal{E}} u_p^2},$$
(37)

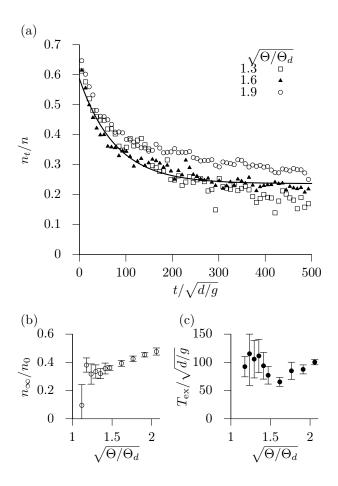


FIG. 10: (a) Time decay of the fraction of grains with an initial velocity above $\sqrt{gd}/2$ that remain in the transport layer, for different shear velocities. The solid line is the exponential fit (Eq. 38) of the data for $\sqrt{\Theta/\Theta_d} = 1.6$ (•). Panels (b) and (c) respectively show the ratio of the asymptotic to initial value and the characteristic exchange time, as a function of the rescaled shear velocity.

The time evolution of n_t in our numerical simulations is displayed in Fig. 10 (a). It can be seen that $n_t(t)$ follows an exponential relaxation with time

$$n_t(t) = (n_0 - n_\infty) \exp\left(-t/T_{\text{ex}}\right) + n_\infty,$$
 (38)

where n_0 and n_{∞} are the initial and asymptotic values, respectively. As the grains that do not move any-more have been exchanged with the static phase, the relaxation time of n_t is by definition the exchange time T_{ex} .

When analyzed for different shear velocities, the fraction of grains re-entrained in the flow after being trapped by the bed, which is given by the ratio n_{∞}/n_0 (Fig. 10 (b)), weakly depends on $\sqrt{\Theta}$, except that it seems to tend to zero at the threshold. It is reasonable in that case that all transported grains are eventually trapped by the surface and replaced by new ones. The exchange time is also roughly constant, with a mean value $T_{\rm ex} \simeq 100\sqrt{d/g}$ (Fig. 10 (c)). This time is larger by two orders of magnitude than the saturation time. This means that exchange

VI. CONCLUSIONS

towards saturation.

The aim of this paper was to present a novel numerical approach for sediment transport based on a discrete element method (DEM) for particles coupled to a continuum Reynolds averaged description of hydrodynamics. We have studied the effect of the grain to fluid density ratio ρ_p/ρ_f and showed that we can reproduce both (sub-aqueous) bed load at ρ_p/ρ_f close to unity, where transport occurs in a thin layer at the surface of the static bed, and (aeolian) saltation at large ρ_p/ρ_f , where the transport layer is wider and more dilute.

We have studied the mechanisms controlling steady, or saturated transport. In the bed load case, saturation is reached when the fluid borne shear stress at the interface between the mobile grains and the static grains is reduced to its threshold value. The number of grains transported per unit surface is therefore limited by the available momentum at the bed surface. However, the fluid velocity in the transport layer remains almost undisturbed so that the mean grain velocity scales with the shear velocity u_* . In the saltation case, particles in motion are able to eject others when they collide with the static bed, and saturation is reached when one grain is statistically replaced by exactly another one after collision. As a consequence, the mean grain velocity scales on the shear velocity threshold u_d , independently of u_* . This provides evidence for a strong negative feedback of the moving grains on the flow within the transport layer, where the wind velocity is reduced. In both bed load and saltation regimes, the number of grains transported per unit area is found proportional to the distance to threshold $\Theta - \Theta_d$, with an identical prefactor on the order of $1/d^2$.

We have systematically varied the density ratio in order to reveal the transition between these two transport regimes. This is also relevant for sediment transport in extraterrestrial atmospheres (e.g. Mars, Venus and Titan) [81, 85, 86]. We have shown that the properties of bed load transport are observed when $s \lesssim 10$, whereas those of aeolian saltation are well established when ρ_p/ρ_f is larger than a few hundred. We have finally discussed the saturation transient of sediment transport. Based on the mechanisms identified in the steady case, we have derived expressions for the saturation time and length in the two regimes. In the bed load case, we have also shown that the exchange time, which reflects the time scale associated to exchange of particles between the mobile and static phases is two orders of magnitude larger than the saturation time.

This study could be continued in different directions. First, it would be interesting to look at the case where the bed is non erodible. This situation has been experimentally investigated in the aeolian regime [90], showing a much wider transport layer λ , and new scaling laws for λ , the roughness z_0 and the flux q_{sat} as a function of u_* . Further work should also be done to perform direct measurements of L_{sat} and T_{sat} . However, the study of inhomogeneous or unsteady situations requires a finer implementation of the model, especially for averaging procedures. A third axis is to take into account the turbulent fluctuations and to address the case of suspended transport [91].

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